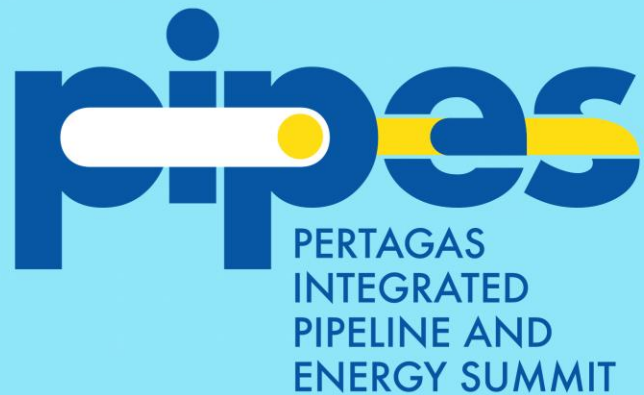




RISK BASED INSPECTION (RBI) & PIPELINE INTEGRITY MANAGEMENT SYSTEM (PIMS) IMPLEMENTATION

PART OF AIMS IMPLEMENTATION

SUMBER	DESKRIPSI	PENGHEMATAN
Jurnal “Risk-based Inspection – Yanbu Gas Plant Study Case Study Module #4 Butane Merox & Caustic Regeneration Module #4 Butane Merox & Caustic Regeneration & Caustic Regeneration Units”, November 2006	Yanbu Gas Plant Engineering melakukan Case Study pada inspection & maintenance yang dilakukan di Saudi Aramco	Penghematan biaya maintenance termasuk Turn Around, sebesar \$11,277M (Rp. 183.476.790.000,-) per tahun setelah menerapkan RBI.
https://www.aoccorp.com/knowledge/rbi-yields-big-savings	Jumlah Equipment yang dioperasikan oleh Gulf Coast Chemical Plant sebanyak 300 Vessels lebih	- Biaya inspeksi tereduksi sebanyak 65% (termasuk biaya persiapan maintenance seperti Scaffolding, Erection, Internal Cleaning dan lain-lain) - Biaya maintenance sebesar \$3,2M (Rp. 52.064.000.000,-) - Optimasi interval Turn Around sehingga menghemat \$8M (Rp. 130.160.000.000,-) - Kurun waktu penghematan : 10 tahun
Studi dari Thesis Universiti Teknologi PETRONAS “Risk Based Inspection on Gas Processing Plant” oleh Mohd Zulfadli Bin Mohd Yunus	Membandingkan antara menerapkan RBI dan tidak pada suatu perusahaan	- Penerapan RBI dapat menghemat cost inspeksi sebesar 410.000 RM (Rp. 1.572.907.600,-) - Penghematan cost dengan penerapan RBI untuk 1 kali Turn Around sebesar 24.000 RM (Rp. 92.072.640,-)

Seluruh area Pertagas mengoperasikan 615 vessels, 27 tanks, 652 PSV, serta lebih dari 1000 piping line pada 150 stasiun, maka peran RBI di Pertagas sangatlah diperlukan.

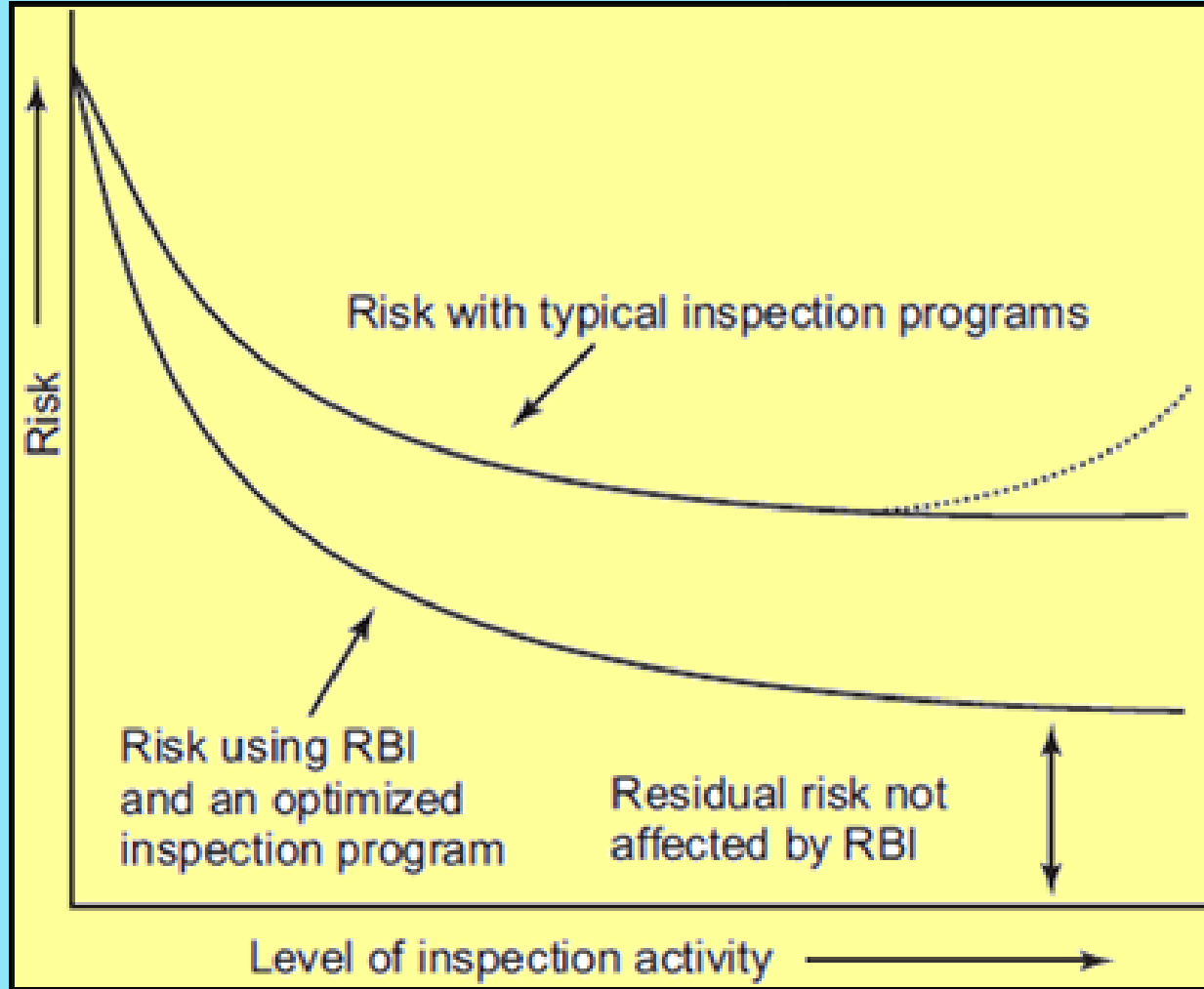
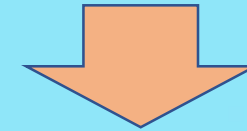
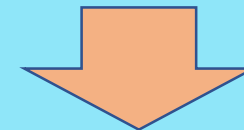


Figure from API 580

Inspeksi API pada dasarnya berbasis pada failure prevention dan tidak mengkonsider konsekuensi dari kegagalan (COF) ataupun potensi kerusakan yang akan terjadi (POF).



RBI Assessment akan menghasilkan Equipment Risk Ranking berdasarkan COF dan POF tersebut dengan output dapat dilakukannya pembuatan strategi operasi dan pemeliharaan berkelanjutan yang optimal.

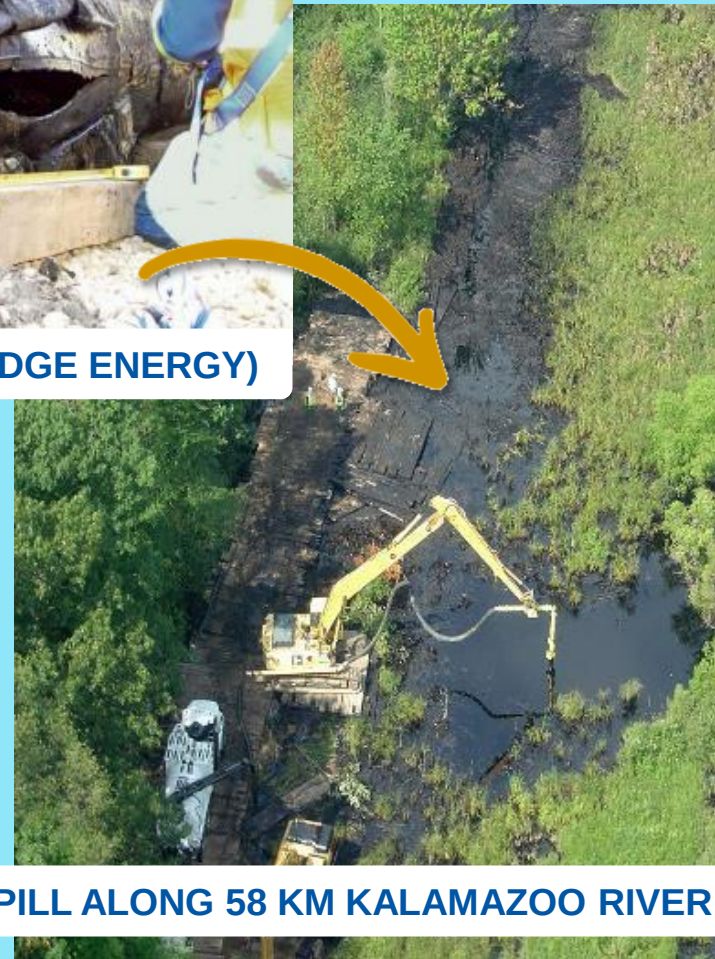


Peningkatan *reliability*, *availability*, dan efisiensi biaya operasi dan pemeliharaan.

Why PIMS



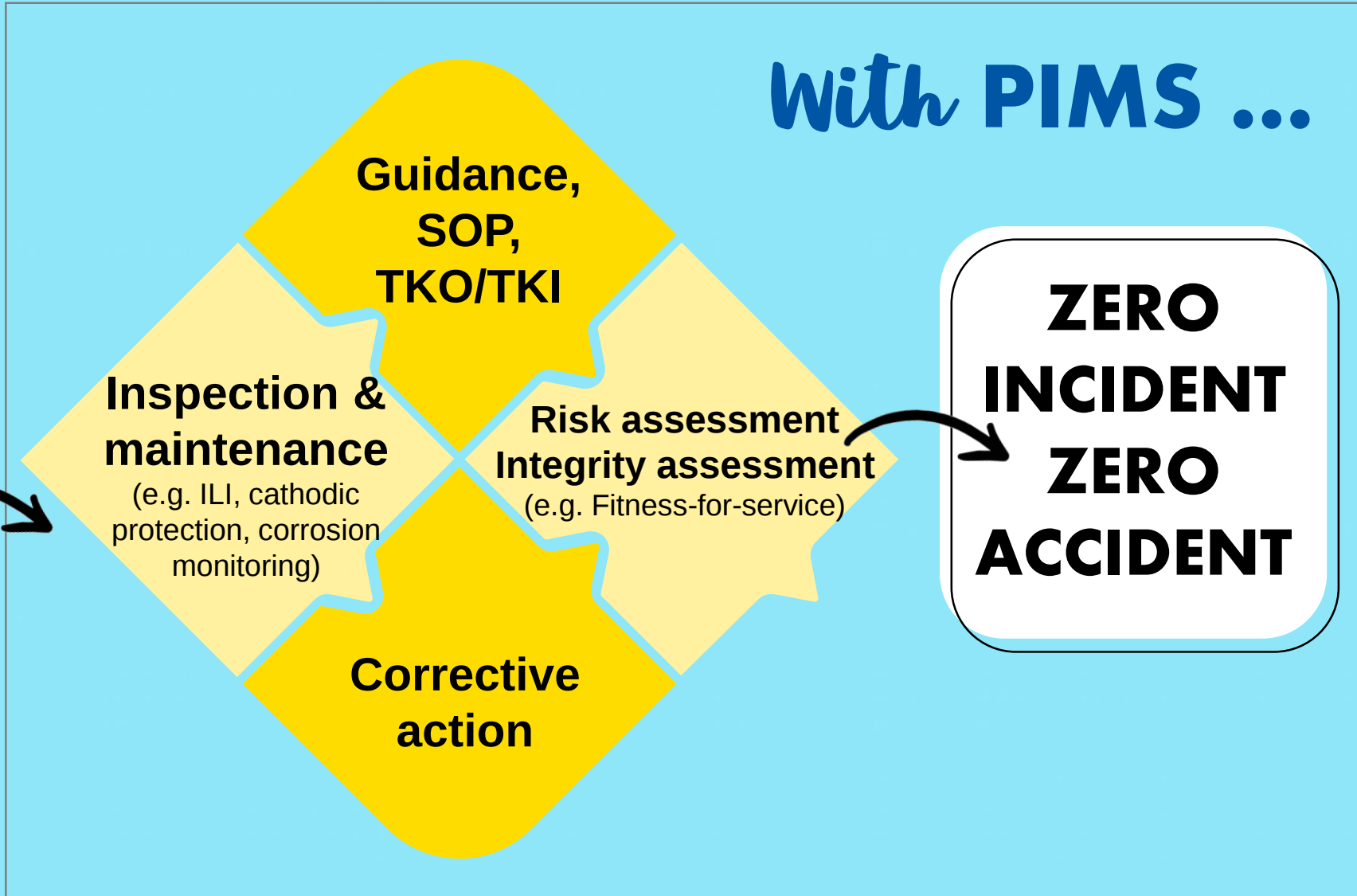
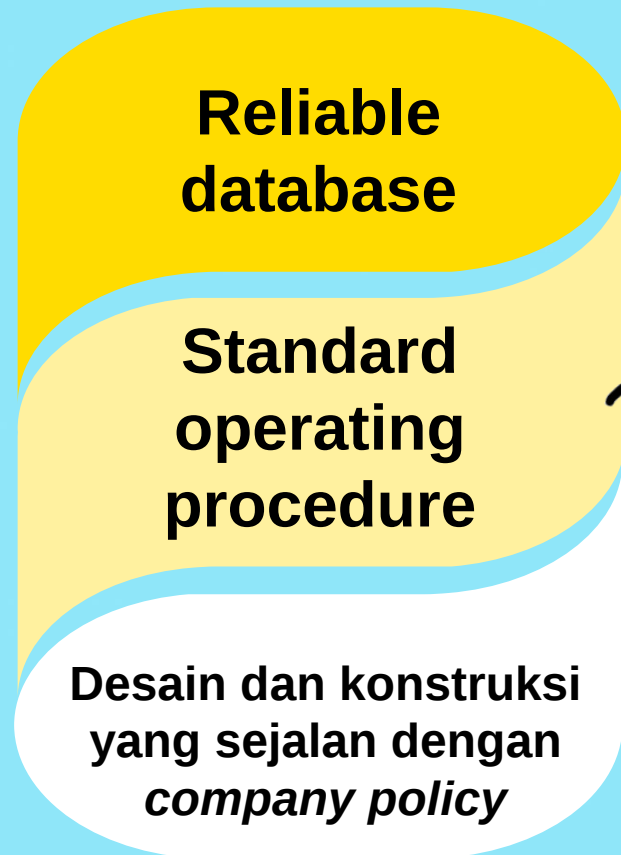
30 INCH PIPE RUPTURE (ENBRIDGE ENERGY)



DILUTED BITUMEN OIL SPILL ALONG 58 KM KALAMAZOO RIVER

Lesson Learned ?

Lesson Learned ?



What reference do we use?

Risk-based Inspection

API RECOMMENDED PRACTICE 580
THIRD EDITION, FEBRUARY 2016

Managing System Integrity for Hazardous Liquid Pipelines

API STANDARD 1160
FIRST EDITION, NOVEMBER 2001



**Helping You
Get The Job
Done Right.**

ASME B31.8S-2004
(Revision of ASME B31.8S-2001)

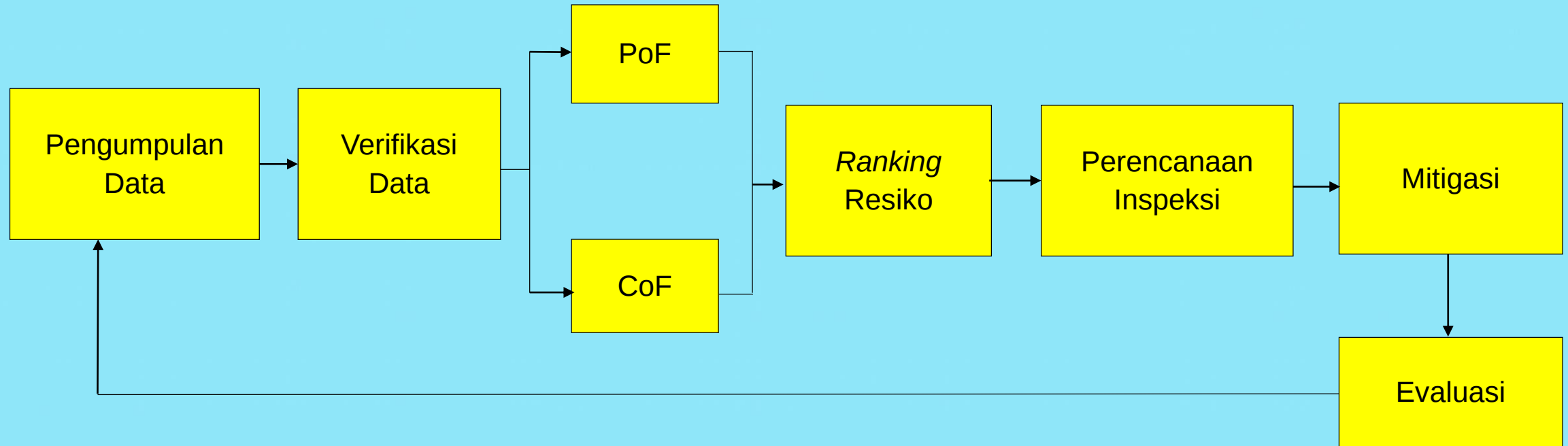
Managing System Integrity of Gas Pipelines

ASME Code for Pressure Piping, B31
Supplement to ASME B31.8

AN AMERICAN NATIONAL STANDARD



Three Park Avenue • New York, NY 10016



Risk Based Inspection (RBI) adalah metode untuk menentukan rencana inspeksi berdasarkan level resiko kegagalan suatu peralatan.

Definisi Kegagalan (Failure): Containment Loss

Risk = Probability of Failure (PoF) × Consequence of Failure (CoF)

	PoF	Risk Matrix				
LIKELIHOOD OF EVENT HAPPENING	5	5	10	15	20	25
	4	4	8	12	16	20
	3	3	6	9	12	15
	2	2	4	6	8	10
	1	1	2	3	4	5
	CoF	1 - Insignificant	2 - Minor	3 - Moderate	4 - Significant	5 - Catastrophic

VERY LOW
 LOW
 MEDIUM
 MEDIUM HIGH
 HIGH

NO	DESCRIPTION	REQUIREMENT	REMARKS
1	Design Basis	Mandatory	Per station
2	Process Flow Diagram (PFD)	Mandatory	Per station
3	Piping and Instrumentation Diagram (PID)	Mandatory	Per station
4	Datasheet Equipment	Mandatory	Per equipment
5	Thickness Measurement Report	Mandatory	Per equipment
6	Gas Analysis Report	Mandatory	Per operated fluid
7	Strength Calculation Report	Complementary	Per equipment
8	GA Drawing Equipment	Complementary	Per equipment
9	Plot Plan	Complementary	Per station
10	Isometric Drawing	Mandatory	For piping
11	Pipe Stress Analysis Report	Complementary	For piping

RBI Assessment Level:

1. Qualitative > applicable to Plant / Station / Unit / Equipment
2. Semi Quantitative > applicable to Equipment
3. Quantitative > applicable to Component

LEVEL 1

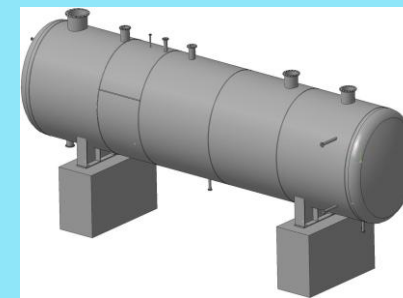
- Fluid Operated (Chemical Compound)
- Total of Equipment
- Potential hazard to equipment, personnel, and environment
- Likelihood Factor

LEVEL 2

The calculation for Level 2 RBI is simpler compared to Quantitative RBI. The Semi-Quantitative approach is applied when a quick risk assessment is required without the use of dedicated software.



Plant



Equipment



Component

POF:

1. Internal Thinning
2. Stress Corrosion Cracking (SCC)
3. External Damage
4. High Temperature Hydrogen Attack (HTHA)
5. Embrittlement
6. Mechanical Fatigue



LEVEL 3



COF:

1. Flammable Consequence
2. Personnel Injury Consequence
3. Toxic Consequence
4. Financial Consequence
5. Non Flammable Non Toxic Consequence



In summary, POF calculation main thing is influenced by:

- | | |
|-------------------------|-----------------------------|
| 1. Chemical Composition | 6. Component Geometry |
| 2. Inspection Result | 7. Interconnected Equipment |
| 3. Inspection Method | 8. Management System |
| 4. Design Pressure | 9. Historical Record |
| 5. Design Temperature | 10. External Intrusion |

In summary, COF calculation main thing is influenced by:

1. Chemical Composition
2. Fluid Volume
3. Operating Pressure
4. Operating Temperature
5. Component Geometry
6. Interconnected Equipment
7. Environmental Data

VAPOR CLOUD EXPLOSION (VCE)



FIREBALL



FLASH FIRE



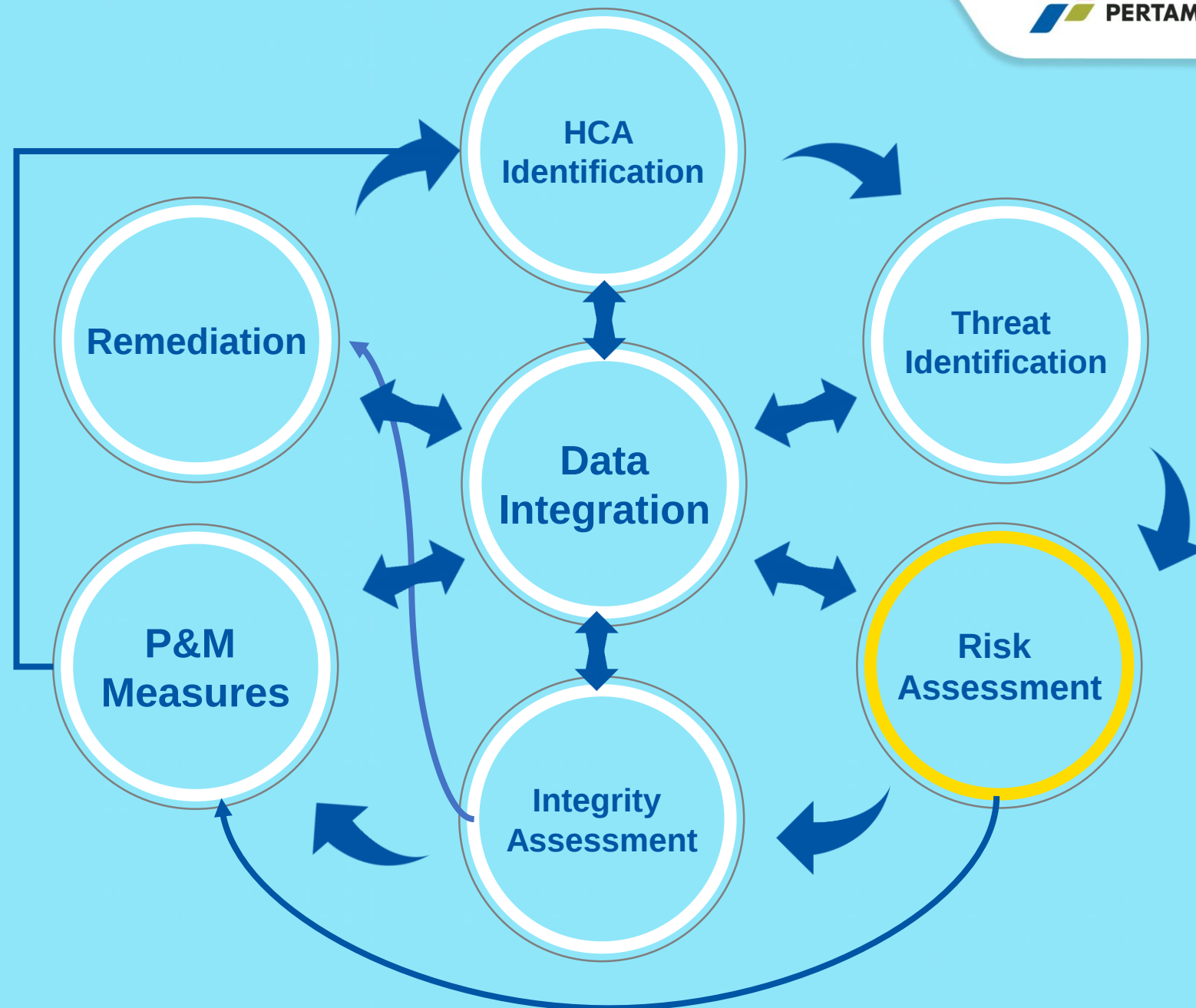
JETFIRE



POOL FIRE



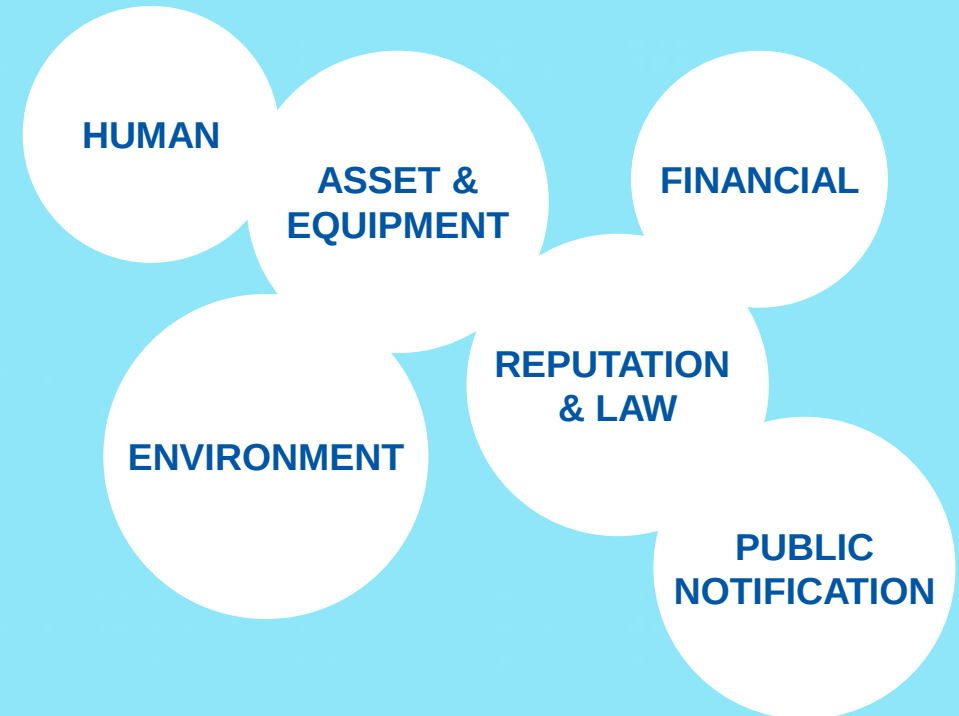
PIMS Cycle



Probability



Consequence





Asset Management



Risk Based
Inspection



Monitored Data



PIMS



RCM



SIL



Anomaly
Management



Preventive
Maintenance



Work Scope



Management
Dashboard



Data Loading



Technical Library



SAP Integration



Menu



PERTAMINA GAS

RBI Engineer



Component Details

Mechanical Design

Process Design

Financial and Prod...

2 Documents

Screening

1 RBI Analysis

— Design Data

Design Code ⓘ

ASME VIII DIV 1

Code Year

1977

Set Pressure (kPa)

878.90

Design Pressure (kPa)

1034.00

Manufactured Year

1999 or prior

Length (m)

0.612

— Material Properties

Material Specification

SA-516 - 70

Material Grade ⓘ

70

Material Type

Carbon Steel

Design Temperature (°C)

38

Allowable Stress (kPa)

120750.0000

External Coating Quality

High - Multi Coat Epoxy or Filled Epoxy

Stress Relieve / PWHT ?



Atmospheric Condition

Marine area / Near Cooling Tower

Insulation Available?



Internal Clad / Coating ⓘ



SMY (psi) ⓘ

37709.88

— T-Min Calculation

Base Metal Nominal Thickness (mm) ⓘ

12.700

Component Shape

PV - Ellipsoidal Head

Internal Diameter (mm)

2447.320

Joint Efficiency

Corrosion Allowance (mm)

Structural Req. Thickness (mm)

8 Risk Ranking Summary

Consequence of Failure (CoF)

Internal Corrosion

External Corrosion

3rd Party Damage

Earth Movement

Flooding

Material Failure

Equipment Failure

Incorrect Operation

Risk Matrix

Inspection Interval

3 Recommendation

— Cathodic Protection

1. CIS Impressed Current



2. CIS Impressed Current Alternative



3. DCVG



4. Current Attenuation CAT



5. Pipe to Soil Potential (PSP) Survey



6. AC/DC Interference



7. 4 PIN Resistivity



8. Rectifier Performance

CIS Impressed Current Ranking

Good: On and Off : $> -0.850V$ and On and Off : < -1.2 

CIS Impressed Current Alternative Ranking



DCVG Ranking



Current Attenuation CAT Ranking



Pipe to Soil Potential (PSP) Survey Ranking

Good: $-0.85 V$ to $-1.2 V$ 

AC/DC Interference Ranking

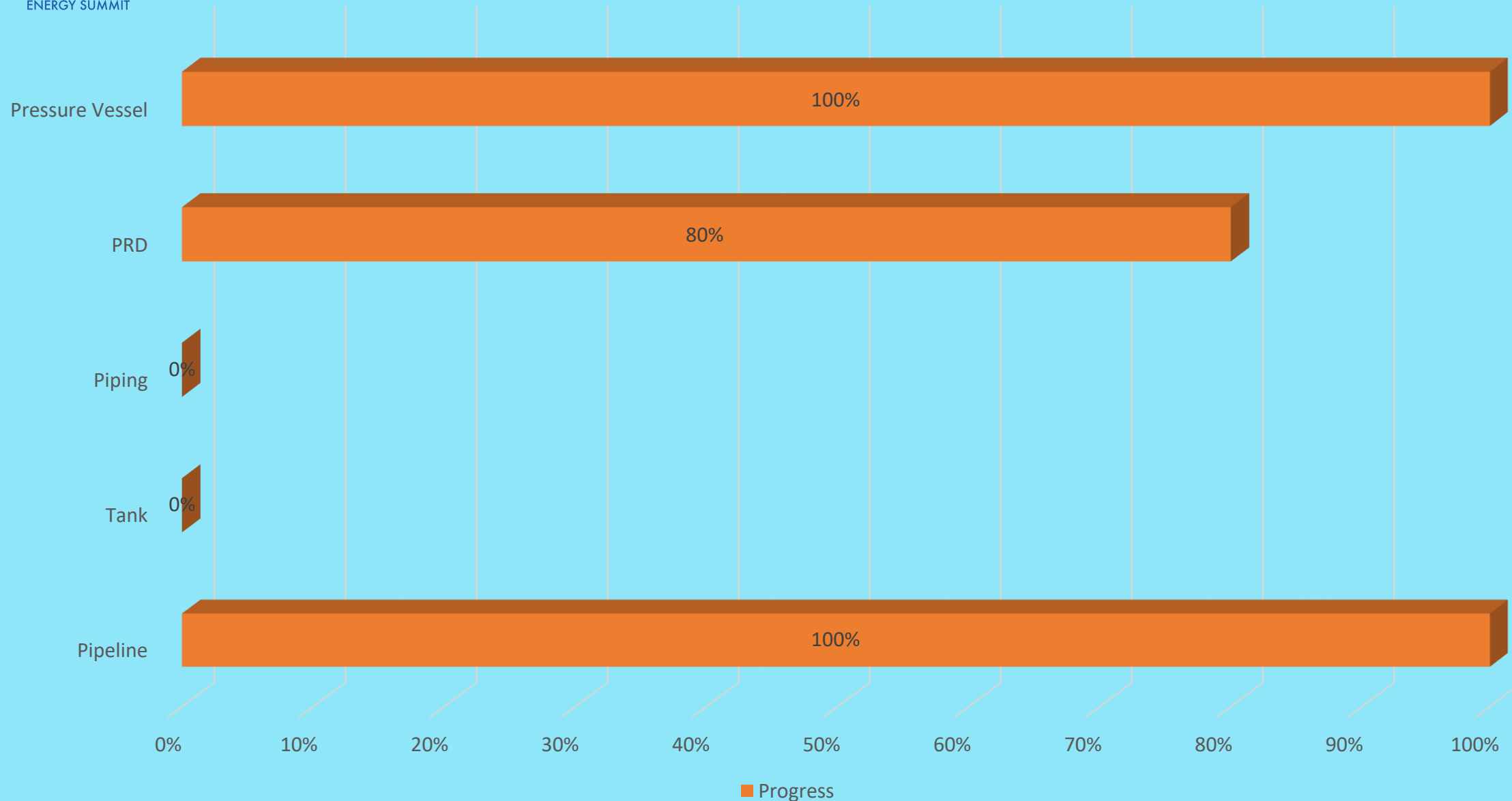


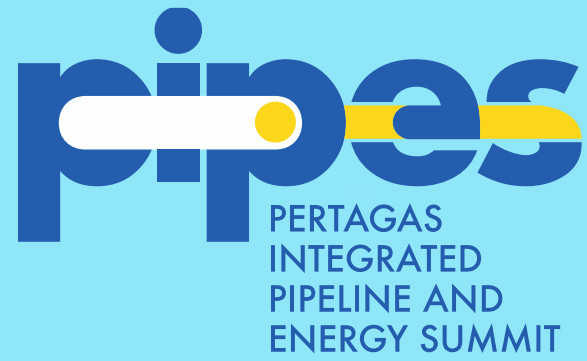
4 PIN Resistivity Ranking

Fair: $1000-10000 \text{ ohm-cm}$ 

Rectifier Performance Ranking

PERTAGAS RBI & PIMS IMPLEMENTATION PROGRESS





**TERIMA
KASIH**